### Dimensionless versus Dimensional Analysis in CFD and Heat Transfer

H. E. Dillon, A. F. Emery, R. J. Cochran, A. Mescher October 2010

### Overview

- Problem Introduction
- Literature Review
- Model (Governing) Equations
- Simulation Results
- Dimensioned and Dimensionless Results
- Conclusions

#### **Problem Introduction**

- There are many ways of non dimensionalizing natural convection flow problems and it is not clear which is best.
- The specific geometry and problem provide a platform to test different methods in COMSOL.

$$A = \frac{H}{R_o - R_i}$$

$$\eta = \frac{Ro}{R_i}$$



### Literature Review

Author	Year	A	Description	
De Vahl Davis 5	1983	1	Benchmark solution for a square cavity.	
Lee and Korpela 9	1983	0-1000	Reported Nu and	
			streamfunctions.	
Chenoweth and Paolucci 2	1986	1 - 10	Compare ideal gas	
			and Boussinesq.	
Suslov and Paolucci 17	1995	$\infty$	Non-Boussinesq impact	
			on stability and considered $Ra_c$ with $\Delta T$ .	
Mlaouah et al. 11	1997	1	Compared Boussinesq, ideal gas,	
			and low Mach approximation.	
Paillere et a. 13	2000	1	Compared Boussinesq	
			and low Mach approximation.	
Xin and Le Quere 20	2002	8	Benchmark study reported $Ra_c$ .	
Christon et al. 3	2002	8	Comparison study of	
Contract Contract			methods, grids, etc.	
Reeve et al. 16	2003	10	Commercial code FIDAP.	
Vierendeels et al. 19	2003	1	Benchmark with ideal gas.	
Xin and Le Quere 21	2006	1-7	Investigated instabilities.	
Dillon et al. 6	2009	8-33	Dimensioned benchmark study	
			in rectangular cavity, COMSOL.	

W UNIVERSITY of WASHINGTON

#### **Problem Introduction**





# Model Equations

Navier Stokes

$$\rho \frac{\partial u}{\partial t} + \rho (u \cdot \nabla) u =$$

$$\nabla \cdot (-pI + \eta (\nabla u + \nabla u^{T}))$$

$$-(2\eta/3 \nabla \cdot u)I + F$$
(5)

Conservation of Mass

$$\nabla \cdot u = 0 \tag{6}$$

Conservation of Energy

$$\rho c_p \frac{\partial T}{\partial t} + \nabla \cdot (-k \nabla T) = -\rho c_p u \cdot \nabla T \quad (7)$$

# Characteristic Velocity Options

Author	Characteristic Velocity	Description
	$\frac{\alpha}{L} = \frac{k}{\rho c_p L}$	Thermal diffusion velocity.
De Vahl Davis 5	$\frac{\sqrt{\beta g \Delta TL}}{\sqrt{Gr}} = \frac{\mu}{\rho L}$	Viscous diffusion velocity.
Ostrach 12	$\sqrt{\beta g \Delta T L}$	For strongly coupled flows $Pr < 1$ and $\sqrt{Gr} > 1$
Ostrach 12	$\frac{\sqrt{\beta g \Delta T L}}{\sqrt{Pr}}$	For strongly coupled flows $Pr > 1$ and $\sqrt{Gr} > 1$
Wan Hassan 8	$\frac{\alpha Ra^{1/4}}{L} = \frac{kRa^{1/4}}{\rho c_p L}$	Based on boundary layer thickness and thermal diffusion velocity.
Abrous 1	$\frac{\mu Ra^{1/4}}{\rho L}$	Based on boundary layer thickness and viscous diffusion velocity.

## Dimensionless Variables

Parameter	Option 1	Option 2	Option 3	
		Strongly coupled	Weakly coupled	
R, Z U	$\frac{\frac{r}{H}, \frac{z}{H}}{\frac{u}{\frac{\alpha}{L}\sqrt{RaPr}}}$	$\frac{\frac{r}{H}, \frac{z}{H}}{\sqrt{q\beta\Delta TH}}$	$\frac{\frac{r}{H}, \frac{z}{H}}{\frac{u}{u_{forced}}}$	
V	$\frac{\frac{v}{\frac{\alpha}{L}\sqrt{RaPr}}}{\frac{\alpha}{L}}$	$\frac{\sqrt{v}}{\sqrt{g\beta\Delta TH}}$	$\frac{v}{u_{forced}}$	
Θ	$\frac{T - T_c}{\Delta T}$	$\frac{\dot{T}-T_c}{\Delta T}$	$\frac{T-T_c}{\Delta T}$	
$\tau$	$t\sqrt{g\beta}\Delta TH^{-1}$			
Р	$\frac{pL}{\mu \frac{\alpha}{L} \sqrt{RaPr}}$			
ρ	$\sqrt{\frac{Ra}{Pr}}$	1	1	
$c_p$	Pr	1	1	
$\mu$	1	$\sqrt{\frac{Pr}{Ra}}$	$\frac{1}{Re}$	
g	1			
$\beta$	1	1	NA	
k	1	$\frac{1}{\sqrt{RaPr}}$	$\frac{1}{Pe}$	
F	$(T-T_c)\sqrt{\frac{Ra}{Pr}}$	$\sqrt{\frac{Ra}{Pr}}$	Re	

## **Dimensioned Variables**

Description	Equation
Boussinesq Approximation	$\rho = \rho_o (1 - \beta (T - T_c))$
Ideal Gas	$\rho = P/RT$
Force Term	$F = -g\rho$

W UNIVERSITY of WASHINGTON

#### Simulation Results



Figure 1: Dimensionless temperature at the center of the cavity over time. Ra = 2.5e7, A = 10 and  $\eta = 0.6$ .

#### Simulation Results



Fig. 2: Sequential contour plot of the stream function illustrating oscillation of the natural convection cells through one period (II). Ra = 2.5e7, A = 10 and  $\eta = 0.6$ .

#### Simulation Results



Fig. 3: Sequential contour plot of the temperature ( $\Theta$ ) illustrating oscillation of the natural convection cells through one period ( $\Pi$ ). Ra = 2.5e7, A = 10 and  $\eta = 0.6$ .

# Dimensioned and Dimensionless Results

Description	Rayleigh	Density	$\mathbf{k},cp,\mu$	Period	Amplitude
Option 1 $16$	2.5e7	Boussinesq	Constant	16.15	0.1285
Option 1	2.5e7	Boussinesq	Constant	16.126	0.1278
Dimensioned	2.5e7	Boussinesq	Constant	16.116	0.1279
Dimensioned	2.5e7	Ideal Gas	Constant	16.161	0.1277
Dimensioned	$2.5\mathrm{e}7$	Ideal Gas	T dependent	16.161	0.1253
Option 1	4e7	Boussinesq	Constant	11.0703	0.1484
Dimensioned	4e7	Boussinesq	Constant	11.0091	0.1485
Dimensioned	4e7	Ideal Gas	Constant	11.0091	0.1485
Dimensioned	4e7	Ideal Gas	T dependent	11.0091	0.1481
Option 1	10e7	Boussinesq	Constant	7.1860	0.1361
Dimensioned	10e7	Boussinesq	Constant	7.0917	0.1362

## Conclusions

- Dimensioned and dimensionless solutions in COMSOL show good agreement for Ra=2.5e7 using the Boussinesq approximation.
- As the Rayleigh number is increased (Ra=10e7) the ideal gas solutions follow a separate solution path. This is a function of the chaotic behaviour of the system. This phenomena has also been observed at higher Rayleigh numbers when the Boussinesq approximation is used [16].

# Chaotic behaviour of the System



At high Rayleigh numbers the system becomes chaotic as new harmonics appear. Ra=18e7 is shown.

# Chaotic behaviour of the System



The system shows hysteresis. Depending on the starting point for the simulations different solution paths are found.

## Future Work

• Continue exploration of the chaotic nature of this system.

#### Acknowledgements

Thanks to NSF for the principle funding through Grant 0626533.

Undergraduate student support from Jaeger Dill, Sarah Edwards, and Kimberley Hartman.