An Integrated Numerical-Experimental Approach for Heat Transfer Analysis of Industrial Furnaces

Adorisio A.⁽¹⁾, Adorisio S.⁽¹⁾, Calderisi M.⁽²⁾, Cecchi A.⁽²⁾, Petrone G.⁽³⁾, Scionti M.⁽³⁾, Turchi F.⁽²⁾

(1) Gadda Industrie, Viale A. Olivetti - 10010 Colleretto Giacosa-Ivrea (TO), ITALY
(2) Laboratori Archa, Via di Tegulaia 10/A - 56121 Ospedaletto (PI), ITALY
(3) BE CAE & Test, Viale Africa, 44 – 95129 Catania, ITALY





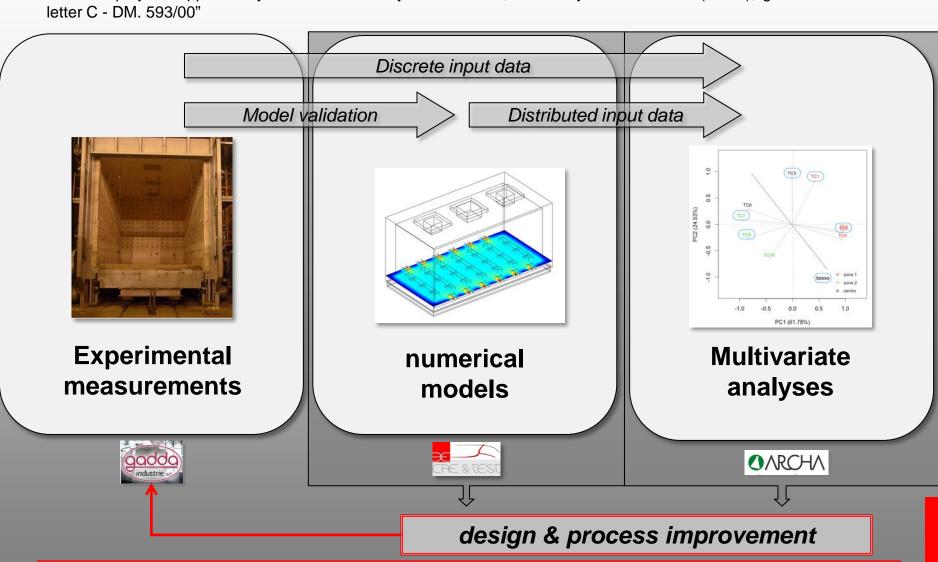


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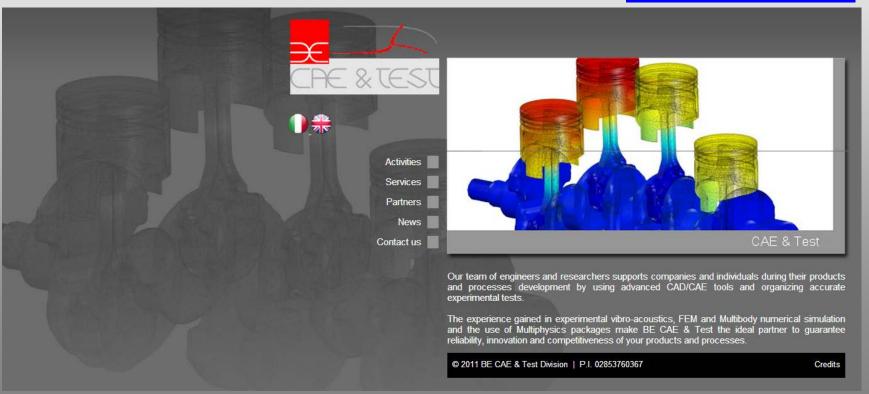


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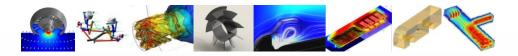
Company profile

- ✓ BE CAE & Test (http://www.be-caetest.it) provides consultancy services in several industrial sectors by using innovative CAD/CAE modelling tools and carrying out experimental campaigns
- ✓ The company collaborates with industrial partners and research centers in several technologic fields.

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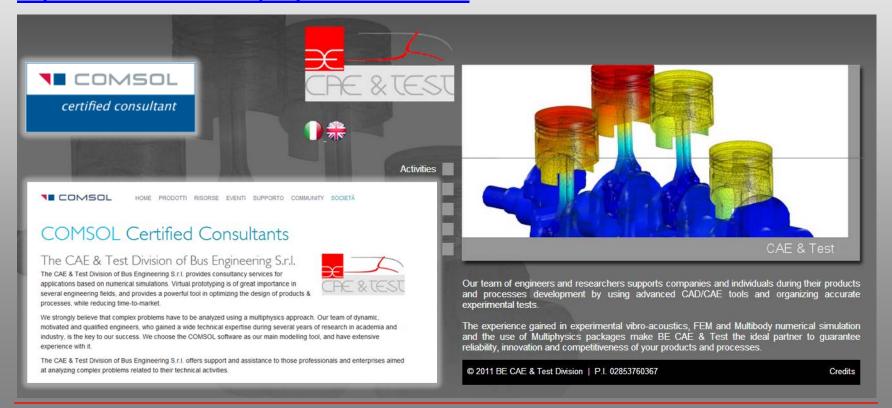




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Partnership

http://www.comsol.it/company/consultants/bus/







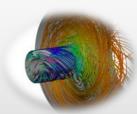


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Fields of activity

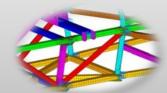
Fluid dynamics and thermal analyses

- Environmental energetics (HVAC, thermal comfort, IAQ)
- Industrial energetics (Thermal design, energy conversion, reacting flows)



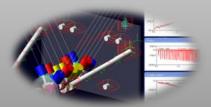
Structural analyses

- Linear and non-linear statics, dynamic and vibro-acustics analyses in industrial and civil applications



System dynamics and Multi-body analyses

- Vehicle and rail dynamics (handling, ride comfort)
- Kinematics, dynamics, rigid and flexible bodies analyses of mechanisms



Experimental testing

- Ride comfort (NVH), modal analyses
- Human body vibrations (ISO standard)









INTRODUCTION

Technical framework and research target

Heat treatments are used to alter the physical, and sometimes chemical, properties of a material. They involve the use of heating or chilling, normally to extreme temperatures, to achieve a desired result such as hardening or softening of a material

Proper heat treating requires very precise control over temperature, time held at a certain temperature and cooling rate. During the heat treatment it is in fact essential that an uniform thermal load is applied to pieces located inside the furnace at each time step of the process.

As a consequence, furnaces need to be designed in order to avoid undesired spatial gradients of temperature when working.

- ➤ The present study deals with an **integrated numerical and experimental** analysis aiming at the **investigation of thermal distribution inside an industrial furnace** built for metal materials treatments.
- The main goal of the research is to analyze the influence of geometrical and functional parameters on the thermal distribution inside the internal volume of the furnace.







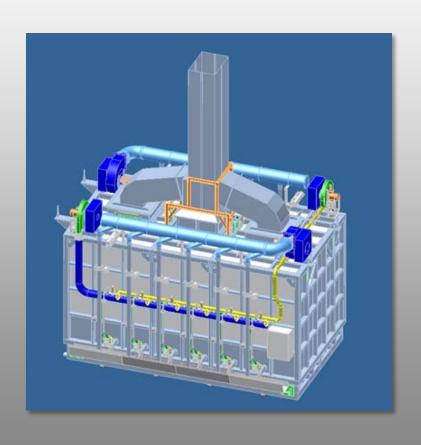


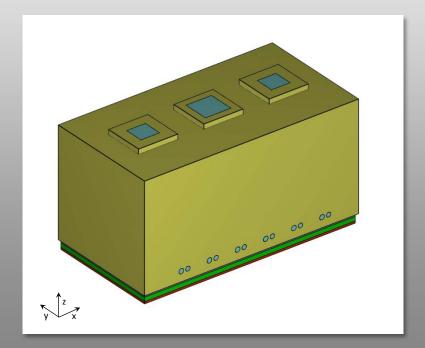




Geometry

Geometry used for computations is derived by the original CAD of the furnace, depurated by all details not strictly needed for fluid-dynamical and thermal simulation



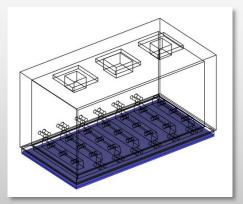




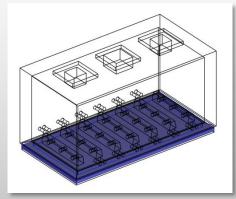




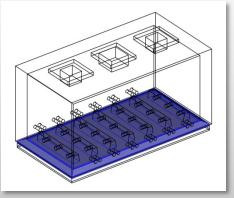
Geometry



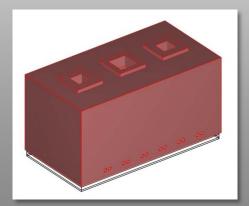
MOSCONI ISO-450 Refractory basement #1



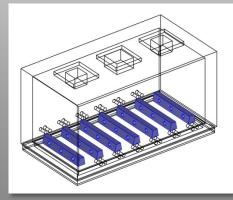
FIR 23 - 0,8 HT Refractory basement #2



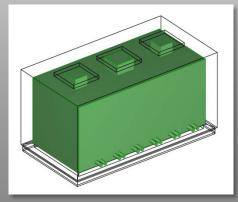
CALDECAST 1560 Refractory basement #3



FIBERFRAX Insultaing layer

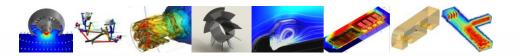


Support for pieces Steel



Air volume Ideal gas







Equations and boundary conditions

Fluid dynamics

Newtonian fluid and uncompressible turbulent flow (k-ε model)

$$\rho \frac{\partial \mathbf{U}}{\partial t} + \rho \left(\mathbf{U} \cdot \nabla \right) \mathbf{U} = \nabla \cdot \left[-p \mathbf{I} + \left(\mu + \mu_T \right) \left(\nabla \mathbf{U} + (\nabla \mathbf{U})^T \right) \right] + F$$

$$\nabla \cdot \mathbf{U} = 0$$

$$\rho \frac{\partial k}{\partial t} + \rho \mathbf{U} \cdot \nabla k = \nabla \cdot \left[\left(\mu + \frac{\mu_T}{\sigma_k} \right) \nabla k \right] + \frac{1}{2} \mu_T \left[\nabla \mathbf{U} + (\nabla \mathbf{U})^T \right]^2 - \rho \varepsilon$$

$$\rho \frac{\partial \varepsilon}{\partial t} + \rho \mathbf{U} \cdot \nabla \varepsilon = \nabla \cdot \left[\left(\mu + \frac{\mu_T}{\sigma_{\varepsilon}} \right) \nabla \varepsilon \right] + \frac{1}{2} C_{\varepsilon 1} \frac{\varepsilon}{k} \mu_T \left[\nabla \mathbf{U} + (\nabla \mathbf{U})^T \right]^2 - \rho C_{\varepsilon 2} \frac{\varepsilon^2}{k}$$



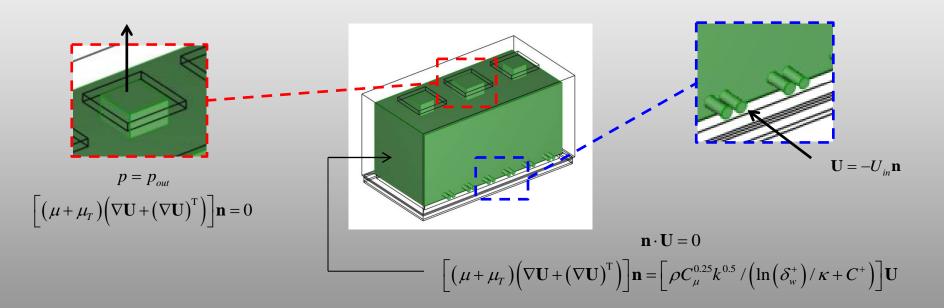




Equations and boundary conditions

Fluid dynamics

Boundary conditions









Equations and boundary conditions

Thermal analysis

Rosseland approximation in order to express the radiating term in the energy equation

$$\rho C_{p} \frac{\partial T}{\partial t} + \rho C_{p} \mathbf{U} \cdot \nabla T = \nabla \cdot \left(\lambda \nabla T\right) + Q + \nabla q_{r}$$

$$\nabla q_{r} = \nabla \cdot \left(\frac{4}{3\kappa_{R}} \nabla E_{b}\right) = \nabla \cdot \left(\frac{4}{3\kappa_{R}} \nabla \left(\sigma T^{4}\right)\right) = \nabla \cdot \left(\frac{16\sigma T^{3}}{3\kappa_{R}} \nabla T\right) = \nabla \cdot \left(\lambda_{R} \nabla T\right)$$

$$\rho C_{p} \frac{\partial T}{\partial t} + \rho C_{p} \mathbf{U} \cdot \nabla T = \nabla \cdot \left((\lambda + \lambda_{R}) \nabla T\right) + Q$$

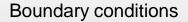


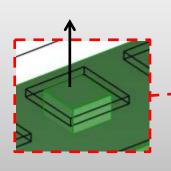




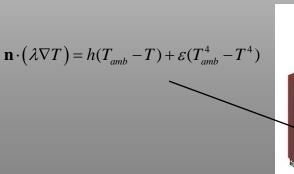
Equations and boundary conditions

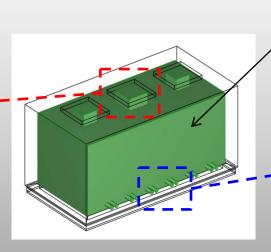
Thermal analysis

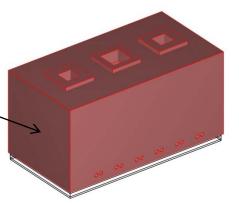


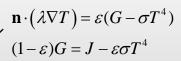


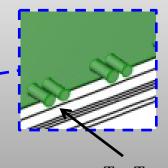
$$\mathbf{n} \cdot (\lambda \nabla T) = 0$$











$$T = T_{in}$$

$$or$$

$$-n \cdot (-\lambda \nabla T) = q_0$$

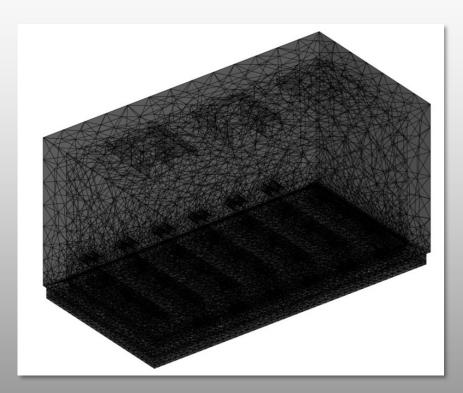






NUMERICAL MODEL Solving

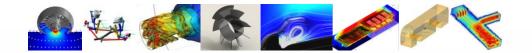
- Continuous equations discretized on nostructured and no-uniform mesh made of tetrahedral Lagrange elements of order 2
- Time-marching performed by an Implicit Differential-Algebraic (IDA) solver based on a variable-order and variable-step-size Backward Differentiation Formulas (BDF)
- Steady solutions achieved by applying an iterative Newton-Raphson algorithm
- Linear system solved by a PARDISO package



Mesh study

Mesh	Mesh #1	Mesh #2	Mesh #3	Mesh #4	Mesh #5
Degree of freedom	61397	87123	108784	151626	228341
Mesh refinement (%)		29.53%	19.91%	28.26%	33.60%
Temperature in (0; 0; 1,5) [°C]	821.3	829.4	835.5	837.4	838.6
Relative gap	2.07%	1.10%	0.37%	0.14%	0.00%

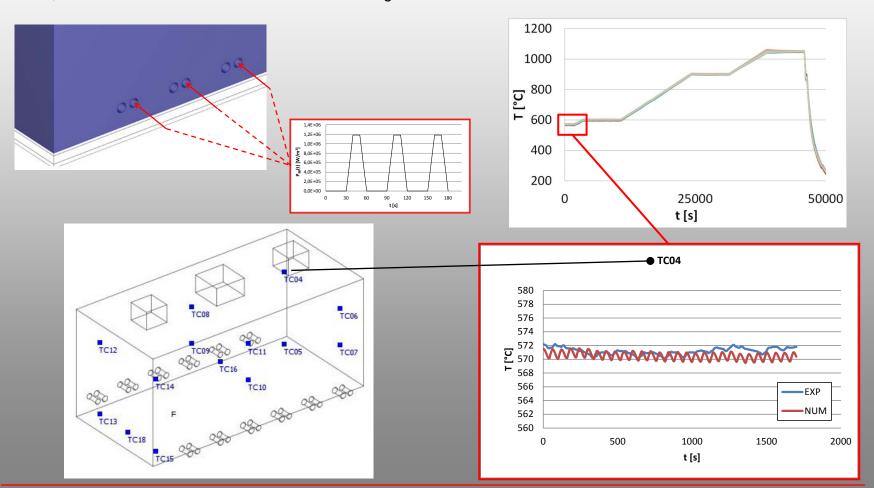






Validation with experimental data (Plateau zone @570 °C)

Computations are carried-out by applying a **periodic thermal flux as thermal input** to the furnace chamber in the FE model, **that simulates** the controlled **ON/OFF** working conditions **for burners**



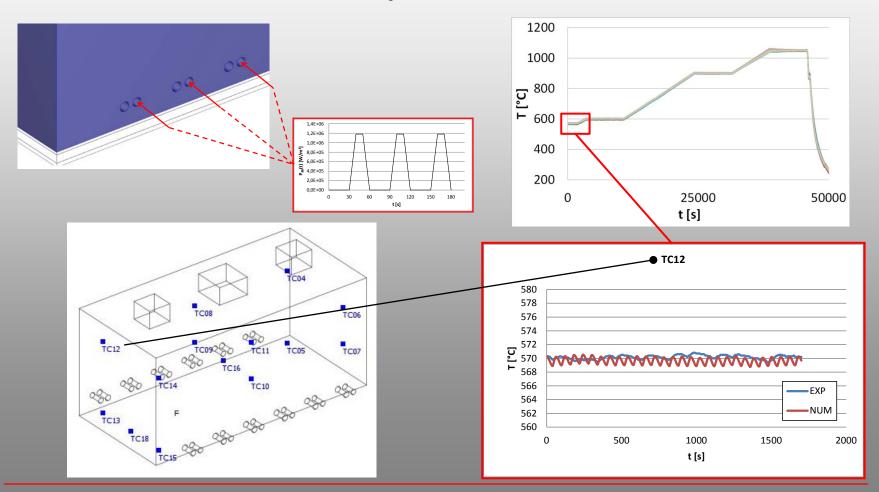






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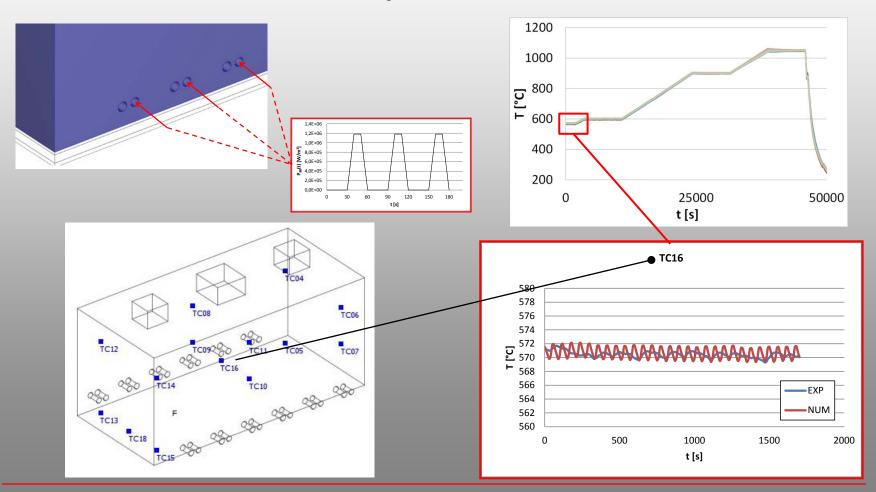






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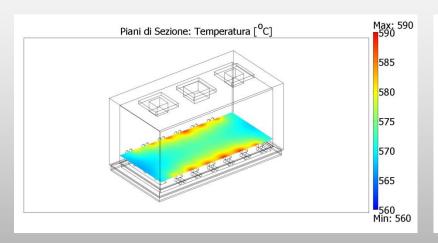


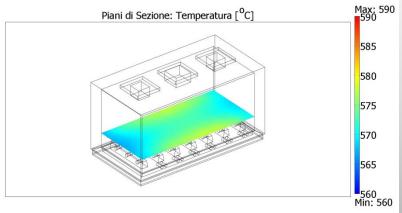


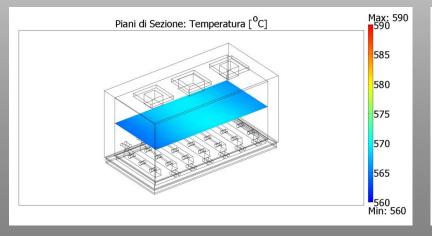


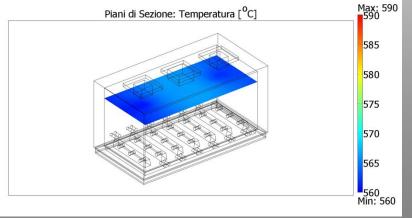
"Base configuration"

√ Thermal distribution in horizontal sections of the chamber









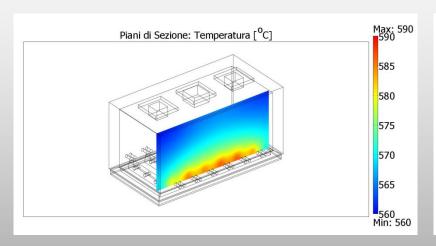


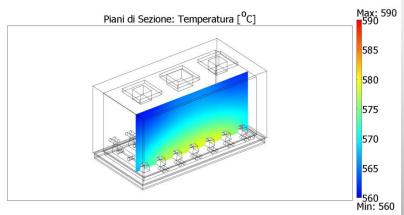


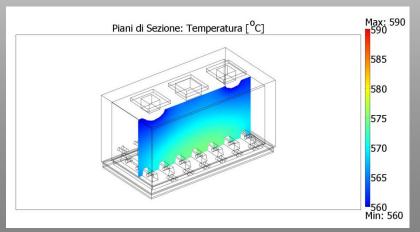


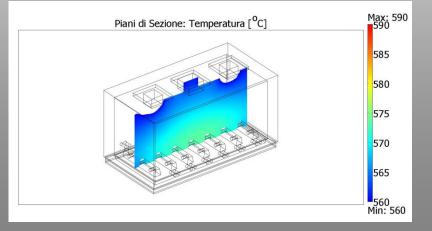
"Base configuration"

√ Thermal distribution in vertical sections of the chamber









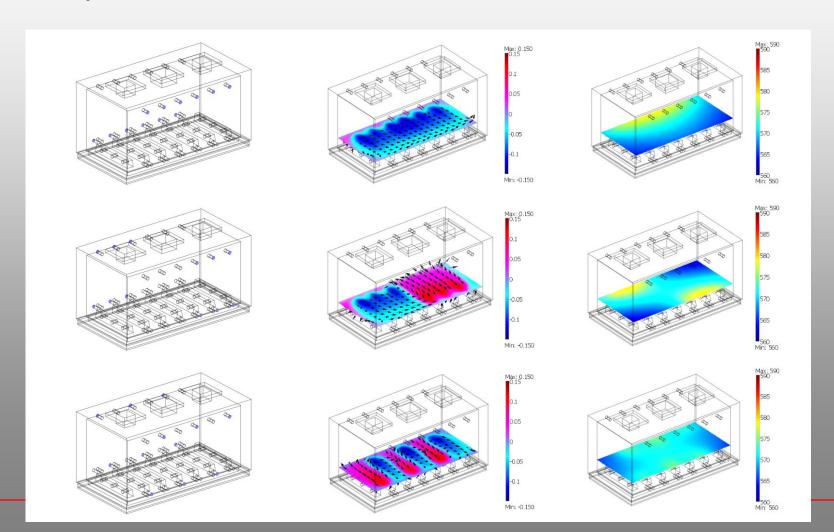






Influence of active burners location

√ Fluid dynamical and thermal distribution in horizontal sections of the chamber



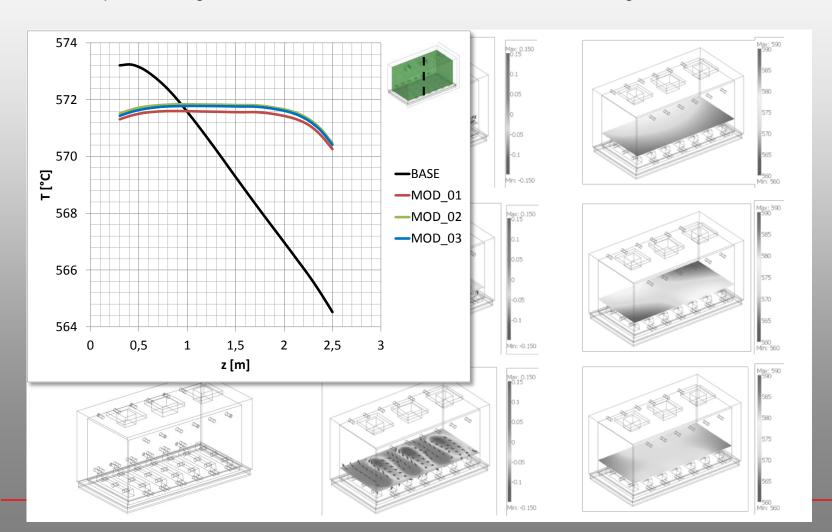




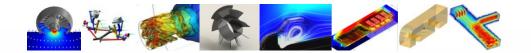


Influence of active burners location

✓ Thermal profile along the z-direction of the chamber for the studied configurations



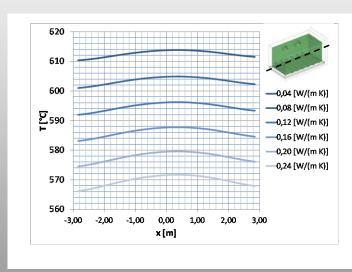


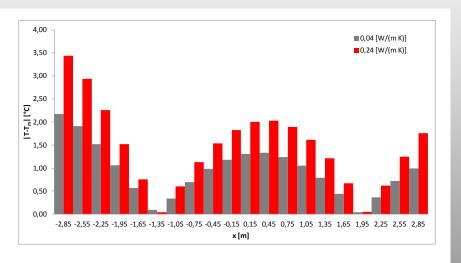




Influence of envelope thermal resistance

- ✓ Temperature profile along the x-direction as a function of the thermal conductivity of the insulating layer
- ✓ Gap between local and average temperature along the x-direction for chosen thermal conductivity values





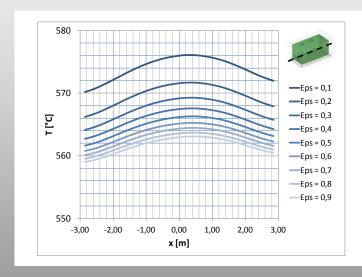


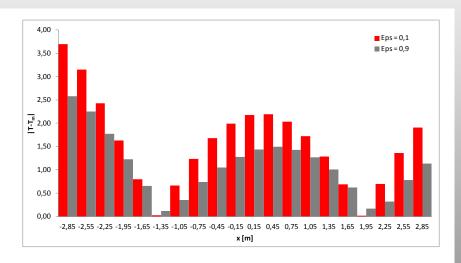




Influence of the internal surface thermal emissivity

- ✓ **Temperature profile** along the x-direction as a function of the **thermal emissivity** of the chamber surface
- ✓ Gap between local and average temperature along the x-direction for chosen thermal emissivity values





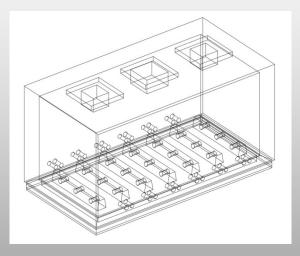


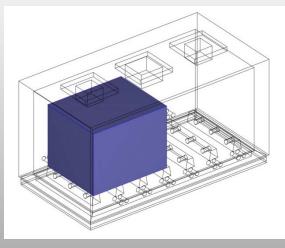


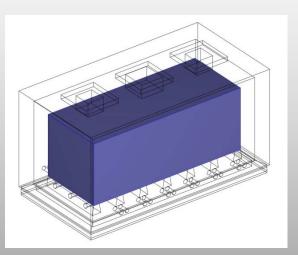


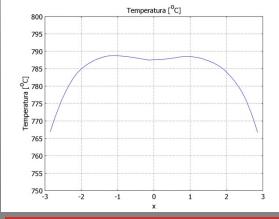
Influence of load

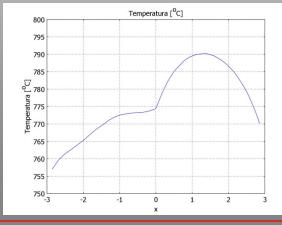
✓ Thermal profile along the x-direction for load-less, half-load and full-load conditions at time instant t=10800 [s] (after 3 hours of heating)

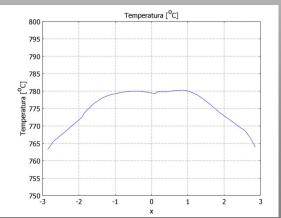












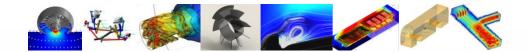






CONCLUSIONS

- An integrated experimental and numerical approach has been exploited in order to assess influence of several geometrical and functional parameters on the internal thermal distribution inside an industrial furnace
- Experimental acquisitions have been used in order to validate FE models as well as input data for statistical analyses based on multivariate regression and unsupervised methods
- Parametrical analyses simulating several working configurations of the device have been carried-out, highlighting optimization criteria related to some design parameters in order to obtain the most homogeneous thermal distribution inside the furnace





BE CAE & TEST

VIALE AFRICA, 44 – 95129 CATANIA (CT)

TEL: +39 095 286 4040

URL: http://www.be-caetest.it
E-mail: info@be-caetest.it

C.F., P.IVA 02853760367 - REA: 303591



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